

Appl. No. 10/814,408  
Atty. Docket: 2002B139/2  
Amendment dated June 20, 2006  
Reply to Office Action dated April 20, 2006

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**Amendment To The Specification**

Please replace paragraph [0113] with the following amended paragraph:

[0113] A preferred embodiment of a riser reactor configuration for use in the present invention is depicted generally as 10 in Figure 1. A methanol feed passed via line 12 is at least partially vaporized in a preheater 14 wherein heat is provided through a heating medium via line 16, controlled by control valve 18. The preheated feed is passed via line 20 and its flow measured by ~~FC-1-22~~ flow controller FC, which measurement is used to derive a signal controlling feed flow control valve 24 for the purpose of controlling methanol feed flow to the riser reactor 26 via feed inlet 28. Control valve 18 is manipulated for the purpose of controlling heat input to the feed by the heating medium in order to control feed preheat rate. One means of measuring the heat content of the feed is by measuring the temperature at ~~TC-1-30~~ temperature controller TC at line 20.

Please replace paragraph [0116] with the following amended paragraph:

[0116] A temperature controller 30 and temperature sensor (TC-2) TC 46, which sensor is positioned at a point in the intermediate portion of the riser reactor between the upper and lower ends of the riser reactor to provide a signal relating to catalyst holdup, with the controller controlling which controls catalyst circulation slide control valve 48 to regulate the flow of regenerated catalyst 50 from regenerator 52. Regenerator flue gas is taken off via line 54, regenerator air is supplied to the reactor via line 56 and coked catalyst is directed from disengaging vessel 34 to regenerator 52 via line 58. Reactor effluent exits disengaging vessel 34 via ~~line 60~~ a reactor effluent line.